

## Chapter 3: Perfect Incompressible Fluid Dynamics

### Introduction:

Fluid dynamics (hydrodynamics) is the science that deals with the behavior of fluids in motion.

In this chapter, we will study fluids in motion by neglecting friction, i.e. by considering them as perfect (zero viscosity) and incompressible (constant density).

### Steady Flow (or Permanent Flow)

A flow is said to be steady (or permanent) when the velocity of the fluid do not change with time at any given point in space.

$$\frac{\partial V}{\partial t} = 0$$

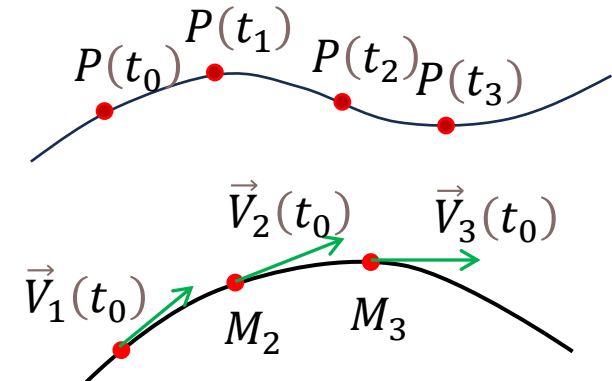
Otherwise, the flow is said to be non-permanent or unsteady.

### The Pathline of particle :

is the curve drawn by the successive positions occupied by the particle over time.

### Stream line:

Is a curve tangent at each point to the velocity vector of the fluid at that instant



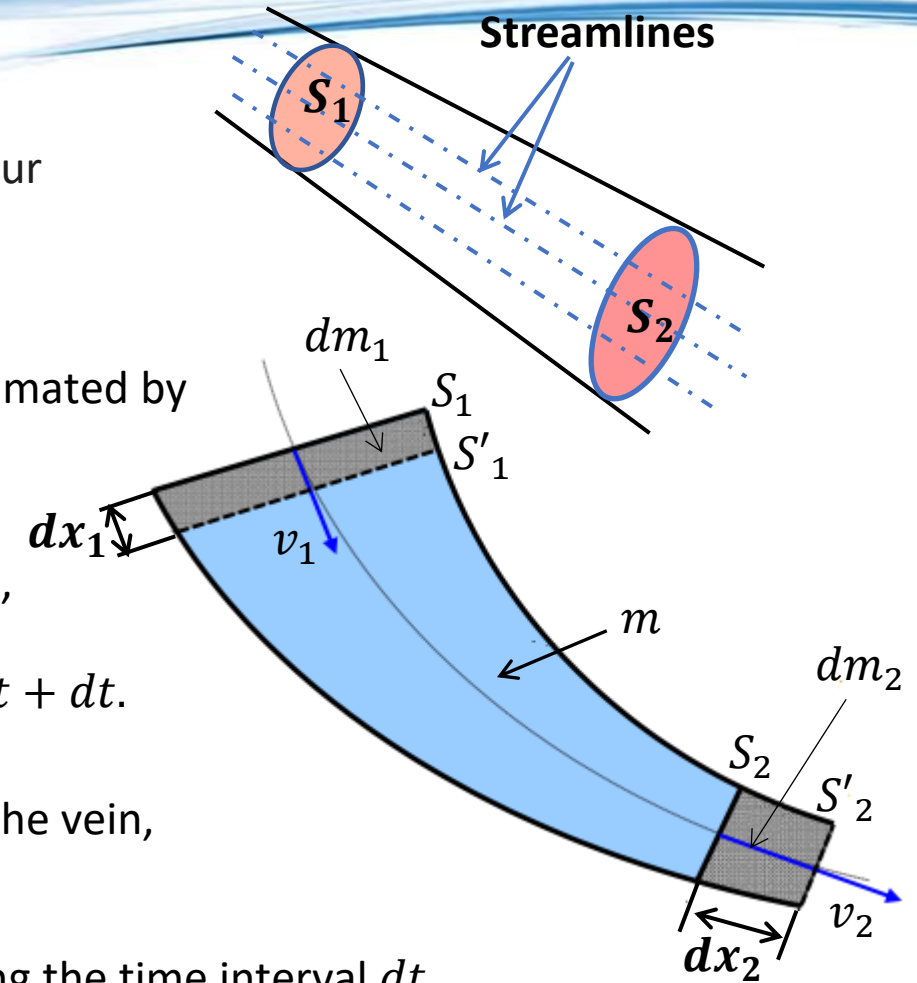
## Stream tube:

A Stream tube is any surface formed by streamlines resting on a closed contour

## Equation of continuity (mass conservation):

Let us consider a vein (conduit) of an incompressible fluid, with a density  $\rho$  animated by a permanent flow. We refer to:

- $S_1$  and  $S_2$  respectively the inlet and outlet cross-section of the fluid at time  $t$ ,
- $S'_1$  and  $S'_2$  respectively the inlet and outlet section of the fluid at time  $t' = t + dt$ .
- $\vec{v}_1$  and  $\vec{v}_2$  are the velocity vectors of flow through the sections  $S_1$  and  $S_2$  of the vein,
- $dx_1$  and  $dx_2$  are respectively the movements of the sections  $S_1$  and  $S_2$  during the time interval  $dt$ ,
- $dm_1$  is the incoming elementary mass between the sections  $S_1$  and  $S'_1$ ,
- $dm_2$  is the outgoing elementary mass between the sections  $S_2$  and  $S'_2$ ,
- $m$  is the total mass between  $S'_1$  et  $S_2$ ,



- $dV_1$  : Elementary volume between sections  $S_1$  et  $S'_1$ ,
- $dV_2$  : Elementary volume between sections  $S_2$  et  $S'_2$ ,
- At time  $t$  : the fluid between  $S_1$  and  $S_2$  has a mass equal to  $(dm_1 + m)$
- At time  $t + dt$  : the fluid between  $S'_1$  and  $S'_2$  has a mass equal to  $(dm_2 + m)$

Let us apply the principle of conservation of the mass of fluid between  $t$  and  $t + dt$  :

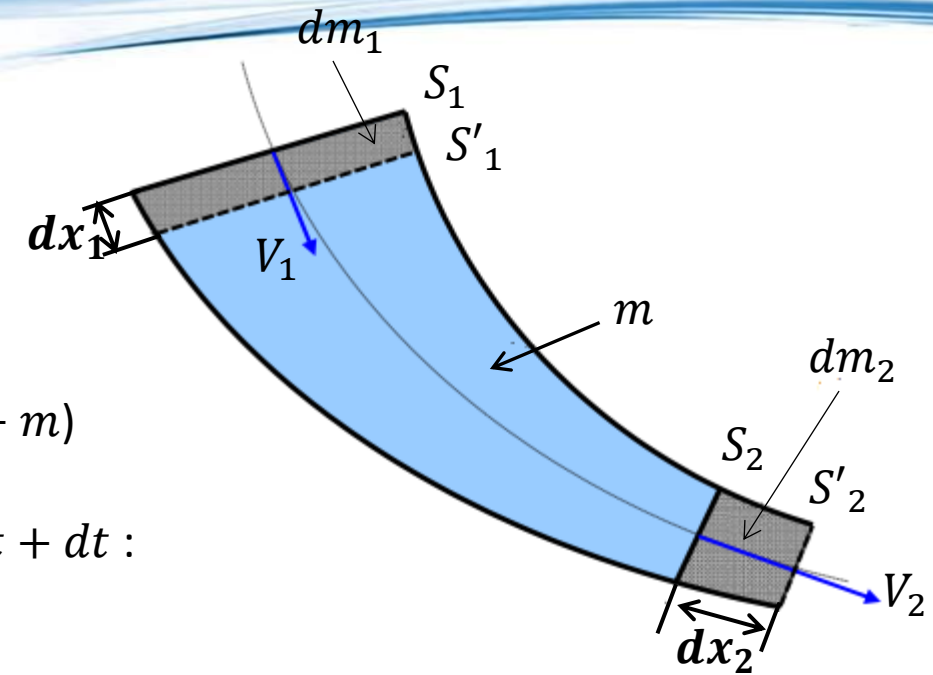
$$dm_1 + m = dm_2 + m \quad \Rightarrow \quad dm_1 = dm_2 \quad \Rightarrow \quad \rho_1 dV_1 = \rho_2 dV_2 \quad \Rightarrow \quad \rho_1 S_1 dx_1 = \rho_2 S_2 dx_2$$

For an incompressible fluid, we have :  $\rho_1 = \rho_2 = \rho \quad \Rightarrow \quad S_1 dx_1 = S_2 dx_2$

Dividing by  $dt$ , we get:

$$S_1 \frac{dx_1}{dt} = S_2 \frac{dx_2}{dt} \quad \Rightarrow \quad S_1 v_1 = S_2 v_2$$

**The continuity equation represents the law of mass conservation**



## Concept of flow rate:

- The flow rate is a quantity of fluid flowed during time  $t$ .
- This quantity can be defined by a volume or a mass.

1. **Mass flow rate:** The mass flow of a fluid vein is the limit of the ratio  $\frac{dm}{dt}$  when  $dt$  tends to 0.

$$q_m = \frac{dm}{dt}$$

$q_m$  is the mass of fluid per unit time ( $Kg/s$ ) which passes through any straight section of the pipe.

$dm$  : The elementary mass in (kg) that passes through the section during a time interval  $dt$  .

$dt$  : Time interval in (s)

Taking into account the **continuity equation** ( $dm_1 = dm_2$ ) , we obtain:  $q_m = \frac{dm}{dt} = \frac{dm_1}{dt} = \frac{dm_2}{dt} = \rho S_1 \frac{dx_1}{dt} = \rho S_2 \frac{dx_2}{dt}$

$$\Rightarrow q_m = \rho S_1 v_1 = \rho S_2 v_2$$

**In general, the mass flow rate is given by:**

$$q_m = \rho S v$$

$\rho$  : density ( $Kg/m^3$ )

$S$  : Fluid Vein Section ( $m^2$ )

$v$  : Fluid velocity through the cross-section  $S$  (m/s)

2. **Volume flow rate:** The volume flow rate  $q_v$  is the elementary volume  $dV$  of fluid that passes through an elementary straight surface  $dS$  during a time interval  $dt$

$$q_v = \frac{dV}{dt}$$

We can also write the volume flow as a function of the flow velocity:

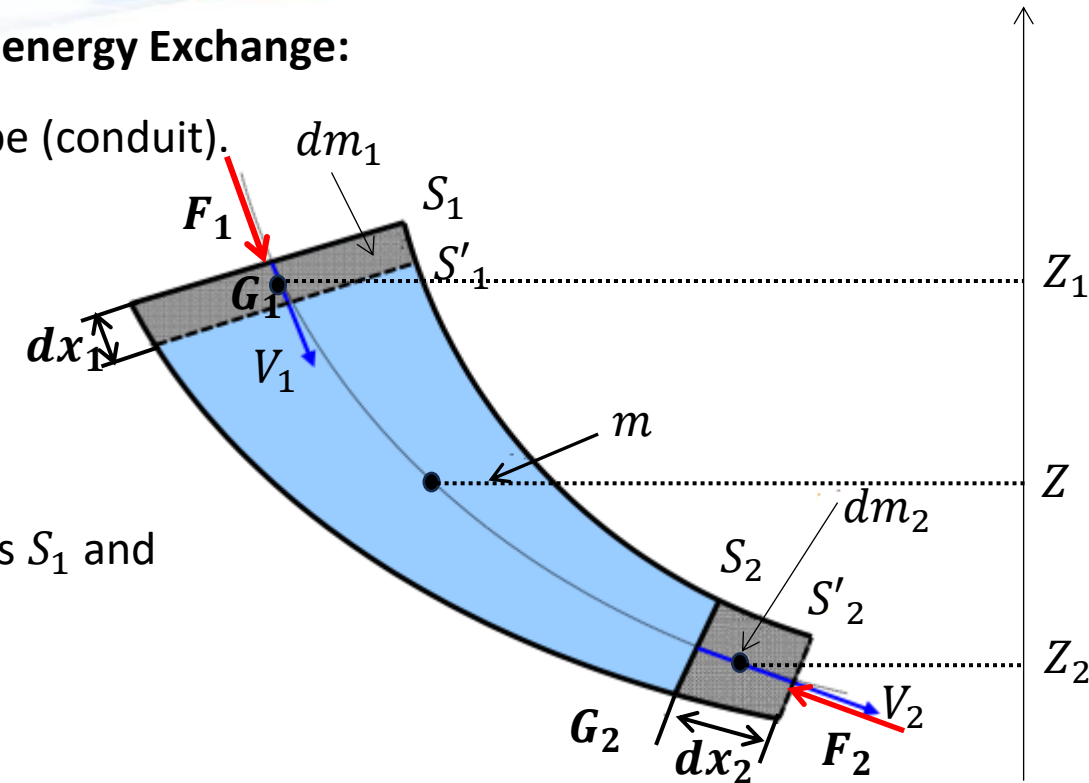
$$q_v = \frac{dV}{dt} = S \frac{dx}{dt} = Sv$$

3. **Relationship between mass flow and volume flow:**

$$q_m = \rho Sv = \rho q_v$$

## Bernoulli's theorem (Conservation of energy)- Case of a Flow without energy Exchange:

- ❖ Let be a permanent flow of an incompressible perfect fluid in a pipe (conduit).
- ❖ The two sections  $S_1$  and  $S_2$  delimit a certain mass of fluid at time  $t$ .
- ❖ we denote  $Z_1$  and  $Z_2$  respectively the heights of the centres of gravity of the masses  $dm_1$  and  $dm_2$ .
- ❖  $F_1$  and  $F_2$  are the norms of the fluid pressure forces acting at sections  $S_1$  and  $S_2$  respectively



Let us apply the kinetic energy theorem to  $dm$ :

$$\Delta E_C(dm) = \sum W_{\vec{F}_{ext}} \quad (\text{The variation in kinetic energy is equal to the sum of the work of the external forces})$$

The variation of kinetic energy:  $\Delta E_C(dm) = \frac{1}{2} dm(v_2^2 - v_1^2)$

The work of the force of gravity:  $W_p = dm \cdot g \cdot (Z_1 - Z_2)$

The work of the inner forces is zero because the fluid is perfect ( $\mu = 0$ )

Work of pressure forces: **On section  $S_1$ :**  $W_1 = F_1 \cdot dx_1 = P_1 \cdot S_1 \cdot v_1 dt$

**On section  $S_2$ :**  $W_2 = -F_2 \cdot dx_2 = -P_2 \cdot S_2 \cdot v_2 dt$

**On the side surface:**  $W_{sd} = 0$

$$\Rightarrow \frac{1}{2} dm(v_2^2 - v_1^2) = P_1 \cdot S_1 \cdot v_1 dt - P_2 \cdot S_2 \cdot v_2 dt + dm \cdot g \cdot (Z_1 - Z_2)$$

$$\Rightarrow \frac{1}{2} \rho \cdot dm(v_2^2 - v_1^2) = P_1 \cdot \rho \cdot S_1 \cdot v_1 dt - P_2 \cdot \rho \cdot S_2 \cdot v_2 dt + dm \cdot \rho \cdot g \cdot (Z_1 - Z_2)$$

According to the equation for the conservation of mass flow:  $dm = \rho \cdot S_1 \cdot v_1 dt = \rho \cdot S_2 \cdot v_2 dt$

$$\Rightarrow \frac{1}{2} \rho \cdot dm(v_2^2 - v_1^2) = P_1 \cdot dm - P_2 \cdot dm + dm \cdot \rho \cdot g \cdot (Z_1 - Z_2) \Rightarrow \frac{1}{2} \rho(v_2^2 - v_1^2) = P_1 - P_2 + \rho g(Z_1 - Z_2)$$

We arrive at Bernoulli's equation:  $P_1 + \rho g Z_1 + \frac{1}{2} \rho v_1^2 = P_2 + \rho g Z_2 + \frac{1}{2} \rho v_2^2 \Rightarrow P + \rho g Z + \frac{1}{2} \rho v^2 = Cte$

The terms of this equation are energies per unit volume [ $J/m^3$ ], These are also pressure terms [ $Pa$ ].

$$\Rightarrow P + \rho gZ + \frac{1}{2}\rho v^2 = Cte$$

### Other forms of Bernoulli's theorem:

□ Dividing the expression by  $\rho g$  we get:

$$Z + \frac{v^2}{2g} + \frac{P}{\rho g} = Cte \quad (\text{in } [m])$$

All terms are unit heights per meter [m] or energy per unit weight

□ Dividing the entire expression by  $\rho$ , we obtain:

$$\frac{1}{2}v^2 + gZ + \frac{P}{\rho} = Cte \quad (\text{en } [J/Kg])$$

All terms are energies per unit mass

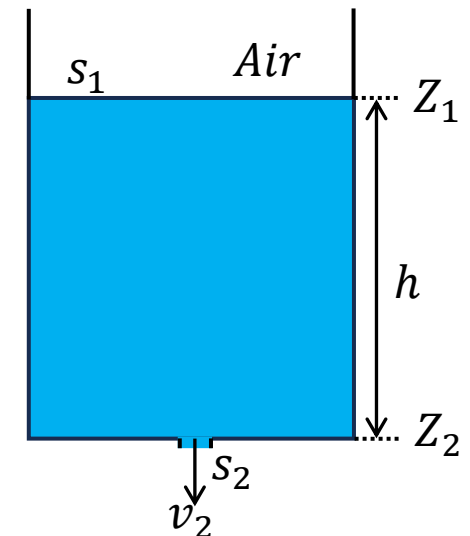
### Applications of Bernoulli's theorem:

#### 1. Emptying a tank (reservoir) (Torricelli's theorem):

We consider a large tank open to the atmosphere containing a liquid of density  $\rho$  and pierced with a small orifice at its base at a height  $h$  of the free surface ( $s_1 \gg s_2$ ).

we apply Bernoulli's theorem between the two surfaces (1) and (2):

$$P_1 + \rho gZ_1 + \frac{1}{2}\rho v_1^2 = P_2 + \rho gZ_2 + \frac{1}{2}\rho v_2^2$$



We have :

$$- P_1 = P_2 = P_{atm}$$

$$- Z_2 = 0, Z_1 = h \text{ (Reference plane in 2)}$$

$$- s_1 \gg s_2 \Rightarrow v_2 \gg v_1 \text{ therefore } v_1 \cong 0$$

We find:  $v_2 = \sqrt{2gh}$  (Torricelli's formula)

### Remark:

If  $s_2$  is not very small compared to  $s_1$ , so we can't neglect  $v_1$

We can then write, according to the continuity equation:  $S_1 v_1 = S_2 v_2 \Rightarrow v_1 = \frac{S_2}{S_1} v_2$

$$\cancel{P_1} + \cancel{\rho g Z_1} + \frac{1}{2} \cancel{\rho} v_1^2 = \cancel{P_2} + \cancel{\rho g Z_2} + \frac{1}{2} \cancel{\rho} v_2^2 \Rightarrow 2gh + v_1^2 = v_2^2 \Rightarrow 2gh + \frac{S_2^2}{S_1^2} v_2^2 = v_2^2$$

$$\Rightarrow 2gh = v_2^2 \left( \frac{s_1^2 - s_2^2}{s_1^2} \right) \Rightarrow v_2 = s_1 \left( \frac{2gh}{s_1^2 - s_2^2} \right)^{\frac{1}{2}}$$



## 2. Venturi tube (Giovanni Battista Venturi (1746–1822)) :

A Venturi tube consists of a narrowing that separates two regions, of different cross-sections ( $S_1$  and  $S_2$  with  $S_1 > S_2$ ), and a horizontal pipeline.

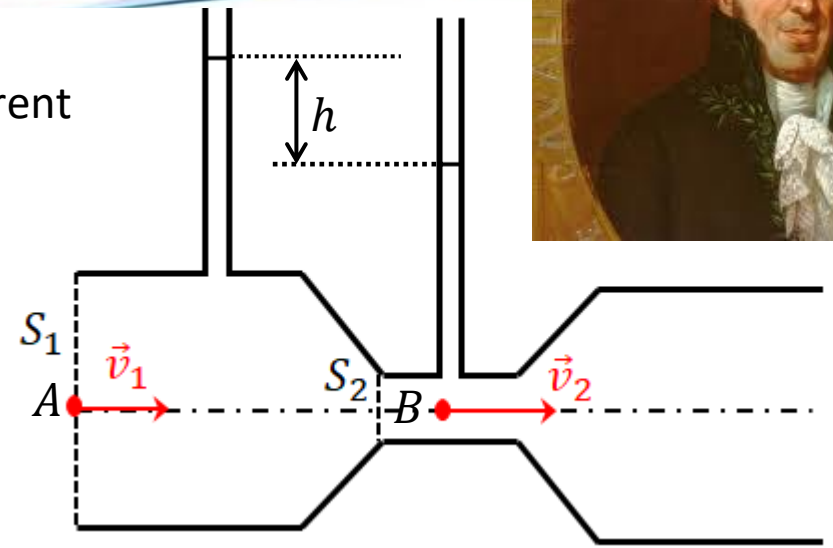
Two vertical tubes emerge from these regions and are open to the air.

- The velocity of the fluid flowing through the pipe increases in the throttle and its pressure decreases ( $v_2 > v_1 \Rightarrow P_2 < P_1$ ).
- Applying Bernoulli's theorem between the two points A and B:

$$P_1 + \rho g Z_1 + \frac{1}{2} \rho v_1^2 = P_2 + \rho g Z_2 + \frac{1}{2} \rho v_2^2 \dots \dots \dots (1)$$

- ✓  $Z_1 = Z_2$  (Same level)
- ✓  $S_1 v_1 = S_2 v_2$  (Continuity equation)  $\Rightarrow v_2 = \frac{S_1}{S_2} v_1$
- ✓ The hydrostatic equation (Pascal's Law) between A and B :  $P_1 - P_2 = \rho g h$

$$(1) \Leftrightarrow P_1 - P_2 = \frac{1}{2} \rho (v_2^2 - v_1^2) = \frac{1}{2} \rho \left( \left( \frac{S_1}{S_2} \right)^2 - 1 \right) v_1^2 \Rightarrow v_1 = \sqrt{\frac{2(P_1 - P_2)}{\rho \left( \left( \frac{S_1}{S_2} \right)^2 - 1 \right)}} \Rightarrow v_1 = \sqrt{\frac{2gh}{\left( \left( \frac{S_1}{S_2} \right)^2 - 1 \right)}}$$



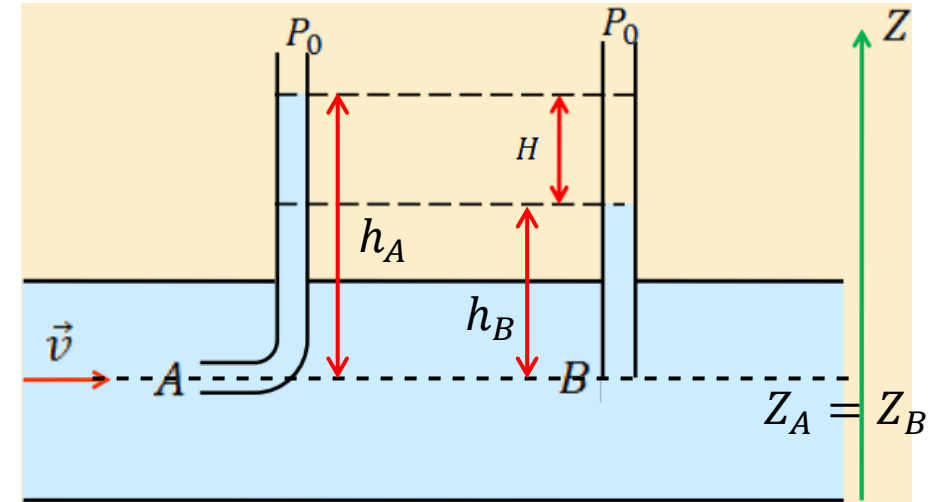
### 3. A Pitot tube (Henri Pitot (1695–1771))



- Consider a pipe with water flowing at a velocity of  $\vec{v}$ ,
- The pipe was fitted with two tubes immersed in the liquid:

One opening at point A facing the flow, and the other at point B aligned with the streamlines. The liquid level difference H between the two tubes was measured.

- At point B:  $\vec{v}_B = v$  (The liquid has the same speed as in the conduit)
- At point A :  $\vec{v}_A = 0$  (stopping point; the flow velocity is zero)
- $Z_A = Z_B$  : points A and B are on the same horizontal plane,



Applying Bernoulli's theorem between the two points A and B:

$$P_A + \rho g Z_A + \frac{1}{2} \rho v_A^2 = P_B + \rho g Z_B + \frac{1}{2} \rho v_B^2 \Rightarrow P_A - P_B = \frac{1}{2} \rho v^2 \dots \dots \dots (2)$$

Applying Pascal's theorem (fundamental relation of hydrostatics):

At point A :  $P_A = P_0 + \rho g h_A$

At point B :  $P_B = P_0 + \rho g h_B \Rightarrow P_A - P_B = \rho g (h_A - h_B) = \rho g H$  ;

$(2) \Leftrightarrow v = \sqrt{2gH}$